

SPECIFICATION AMENDMENTS

On page 1, insert above line 1, insert--Priority Claim

The present application claims priority on European Patent Application
03256832.1 filed October 29, 2003.--

On page 1, above line 1, insert--Field of the Invention--

On page 1, above line , insert--Background of the Invention--

On page 1, above line 26, insert--Summary of the Invention--

On page 2, above line 7, insert--Detailed Description of the Invention--

Paragraph on line 34 of page 3, ending on line 12 of page 4, has been amended as follows:

--Many variations on the above concept are known. These include separation of air into gaseous products, liquid products and all kind of combinations thereof. Also the production of partly enriched oxygen and/or nitrogen streams together with almost pure oxygen and/or nitrogen streams, either in liquid or gaseous phase is well known. In addition there may be additional distillation units to separate any of the rare gases present in the feed air. Further, the methods for creating the low temperatures may vary in many ways. In this respect reference is made to the above cited literature references, and further to ~~EP-A-798524~~ U.S. Pat No. 5,778,698, ~~JP-A-08094245~~, ~~EP-A-593703~~ U.S. Pat No. 5363656, ~~EP-A-562893~~ U.S. Pat No. 5341647, ~~US-A-Pat. No. 5237822~~, ~~JP-A-02052980~~, ~~EP-A-211957~~ U.S. Pat No. 4853015, ~~EP-A-102190~~ U.S. Pat No. 4529425, ~~SU-A-47595~~ ~~JP-A-71020126~~ and ~~JP-A-71020125~~.--

Paragraph on line 13 of page 6 has been amended as follows:

-- Examples of suitable Fischer-Tropsch synthesis processes for step (c) ate for example the so-called commercial Sasol process, the Shell Middle Distillate Process or by the non-commercial Exxon process. These and other processes are for

example described in more detail in EP-A-776959, EP-A-668342, US-A-Pat. No. 4943672, US-A-Pat. No. 5059299, ~~WO-A-9934917~~ U.S. Pat. No. 6130184 and WO-A-9920720 and are incorporated by reference. The Fischer-Tropsch process may be carried out in a slurry reactor, a fixed bed reactor, especially a multitubular fixed bed reactor or in a three phase fluidised bed reactor.--

Paragraph on line 6 of page 7 has been amended as follows:

-- Alternatively the waxy product is subjected to a hydrocracking/hydroisomerisation process wherein lower boiling fractions are obtained, such as for example paraffin products boiling in the naphtha, kerosene and gas oil boiling range. The partly isomerised liquid products so obtained may be shipped to end costumers for use as aviation fuel (blending components), diesel fuel (blending components), industrial gas oil (blending components), drilling fluids, steam cracker feedstock or solvents. The partly isomerised wax as obtained in such process steps may advantageously be further processed by means of dewaxing to obtain lubricating base oils or may be shipped as an intermediate product to base oil manufacturing locations more near to the end users. Examples of such processes are described in more detail in US-A-Pat. No. 6309432, US-A-Pat. No. 6296757, US-A-Pat. No. 5689031, EP-A-668342, EP-A-583836, US-A-Pat. No. 6420618, WO-A-02070631, WO-A-02070629, WO-A-02070627, WO-A-02064710 and WO-A-02070630, which references are incorporated by reference. The referred to hydrocracking/hydroisomerisation and optimal dewaxing steps are thus performed at the remote location and the resulting above described products are the hydrocarbon products to be shipped.--

On page 10, above line 1, insert--We claim:--